

New Sorbent from Agro-industrial Waste and its Potential Use in 17β -Estradiol and 17α -Ethinylestradiol Removal

Suzimara Rovani*, Éder C. Lima, Renato Cataluña, Andreia N. Fernandes

*Institute of Chemistry, Federal University of Rio Grande do Sul (UFRGS), Porto Alegre, RS, Brazil. *suziquimica@gmail.com*

INTRODUCTION

✓ The long-term risks of endocrine disruptors compounds (EDC) still remains unclear for non-target organisms as well as for human health, since EDC can be found in very low concentrations (range of ng L^{-1}) in different environmental compartments.^{1,2}

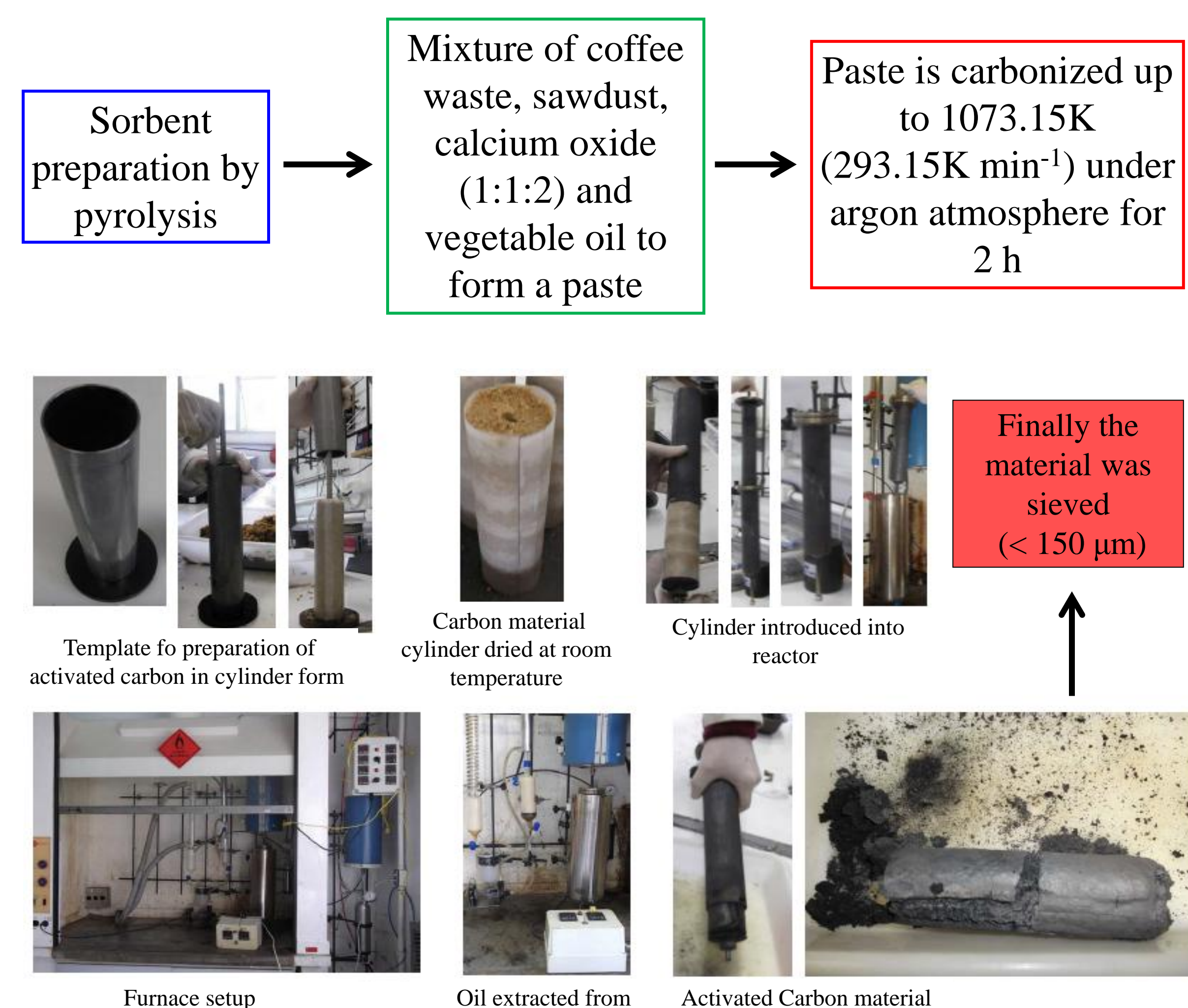
✓ There is a need for developing new reliable analytical methods, which will enable a rapid, sensitive and selective determination of EDC in environmental samples.

✓ Therefore, a sample pretreatment step prior to chromatographic analysis is necessary for pre-concentrating the target analytes.³

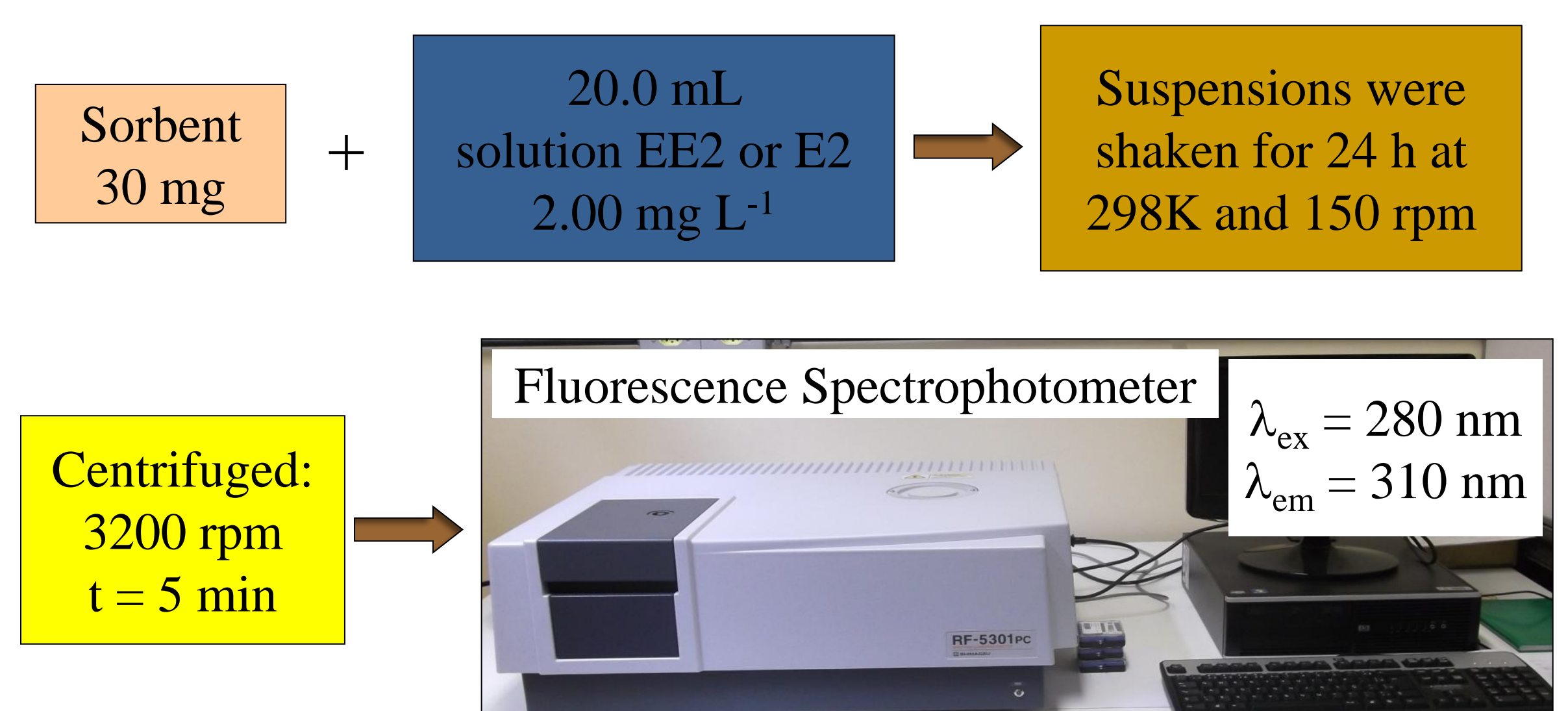
OBJECTIVE: Develop a new sorbent from agroindustrial waste for removal of 17β -estradiol (E2) and 17α -ethinylestradiol (EE2) from aqueous solution.

EXPERIMENTAL

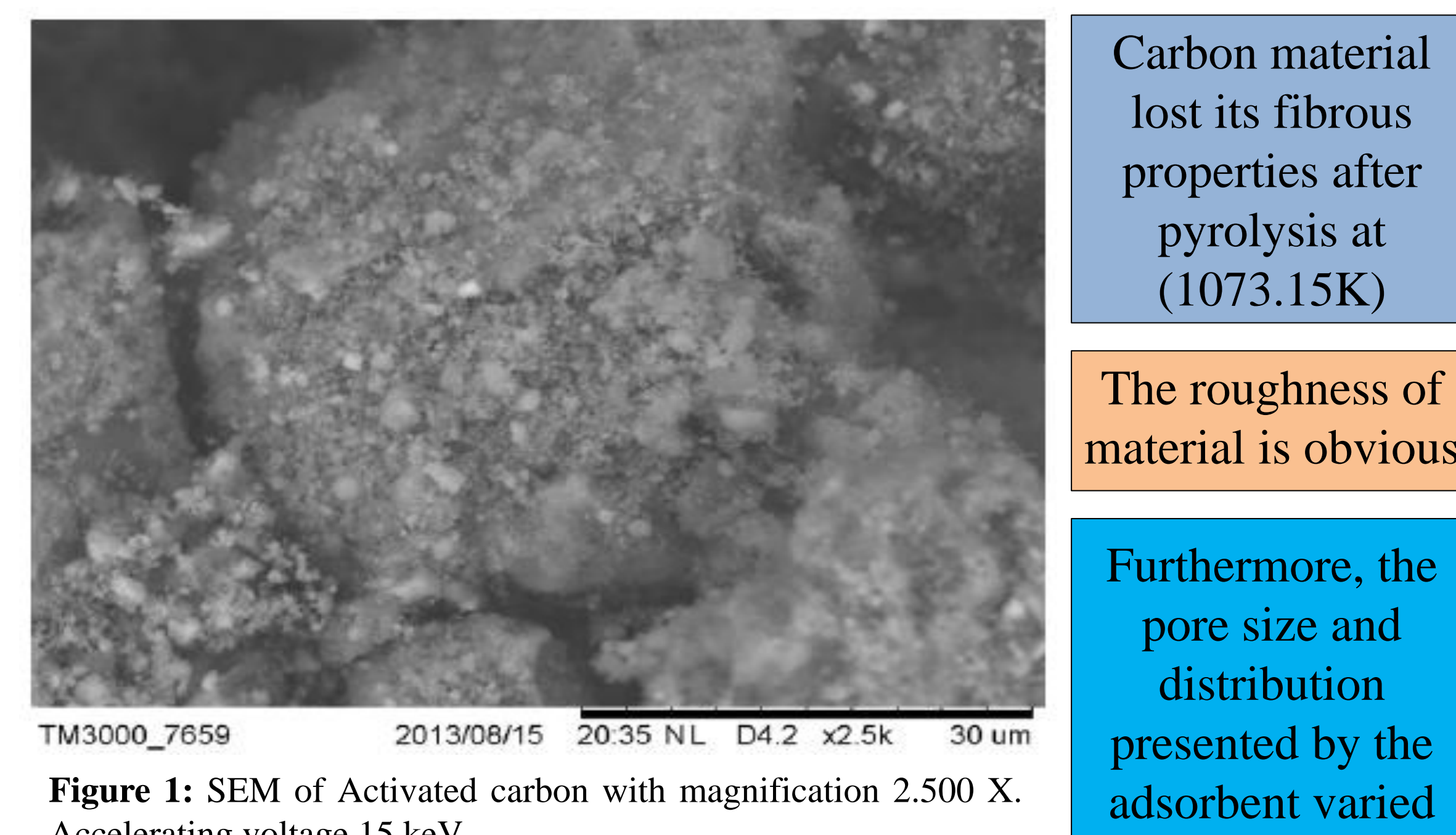
Sorbent Preparation



Removal of 17β -estradiol and 17α -ethinylestradiol



Analysis of SEM



FTIR Vibrational Spectra

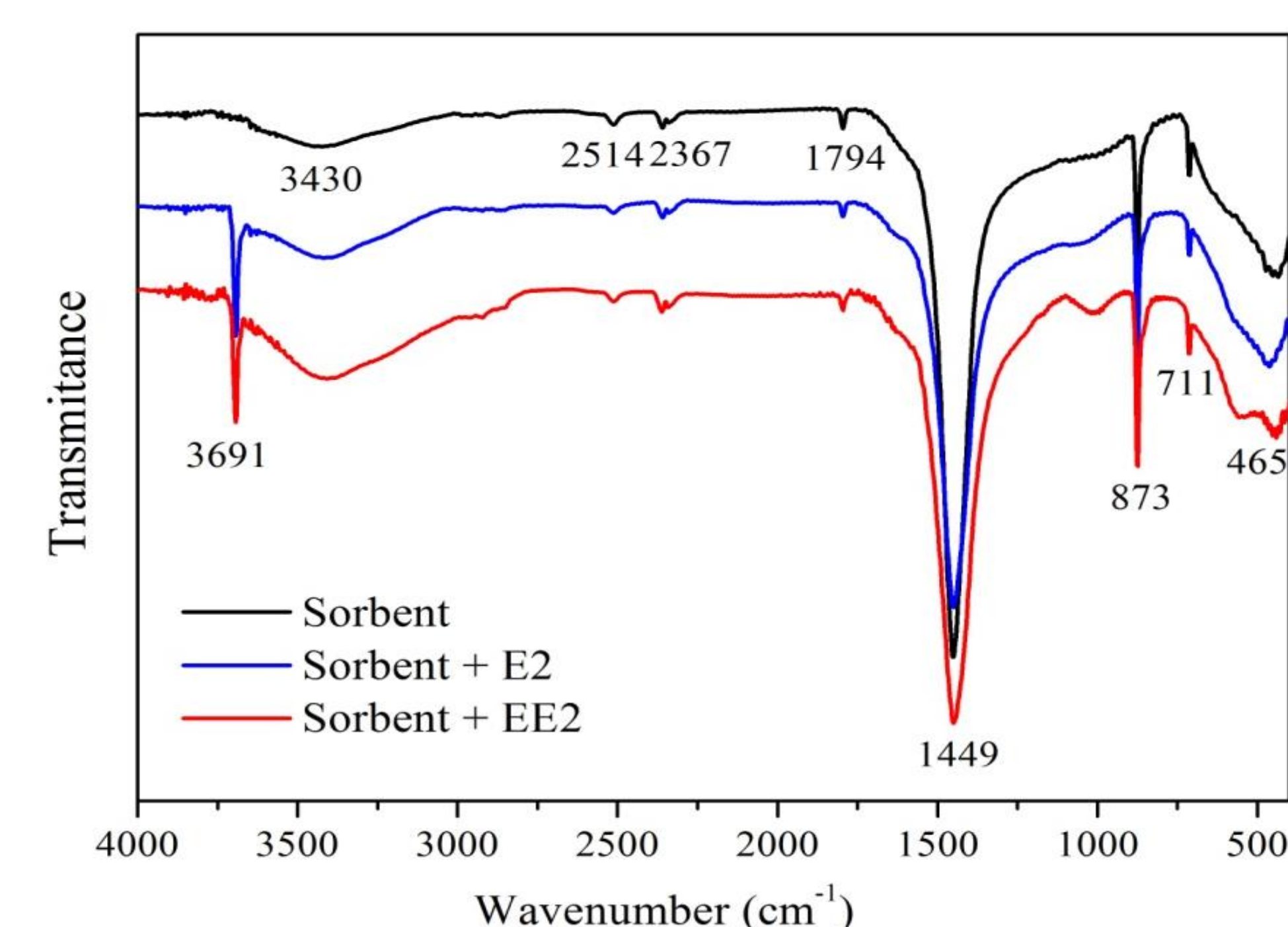


Figure 2: FTIR vibrational spectra. The number indicated for the bands correspond to wavenumbers that are expressed in cm^{-1} .

- 3691 cm^{-1} OH stretch of "free" (no hydrogen bond) of estrogens
- $\sim 3430 \text{ cm}^{-1}$ OH stretching (with hydrogen bond)
- 1794 cm^{-1} C=O bond of the carbonyl groups or carboxylate esters
- 1449 cm^{-1} aromatic rings conjugated with the carbonyl group
- 873 cm^{-1} bending CH

Water Contact Angle (WCA)

- Contact Angle (θ) = $115.22^\circ \pm 0.026$.
- (θ) between 90° and 150° is called the hydrophobic surface.⁴



Figure 3: Measure the water contact angle of the activated carbon.

RESULTS AND DISCUSSION

Point of Zero Charge (pH_{PZC}) - Effect of pH

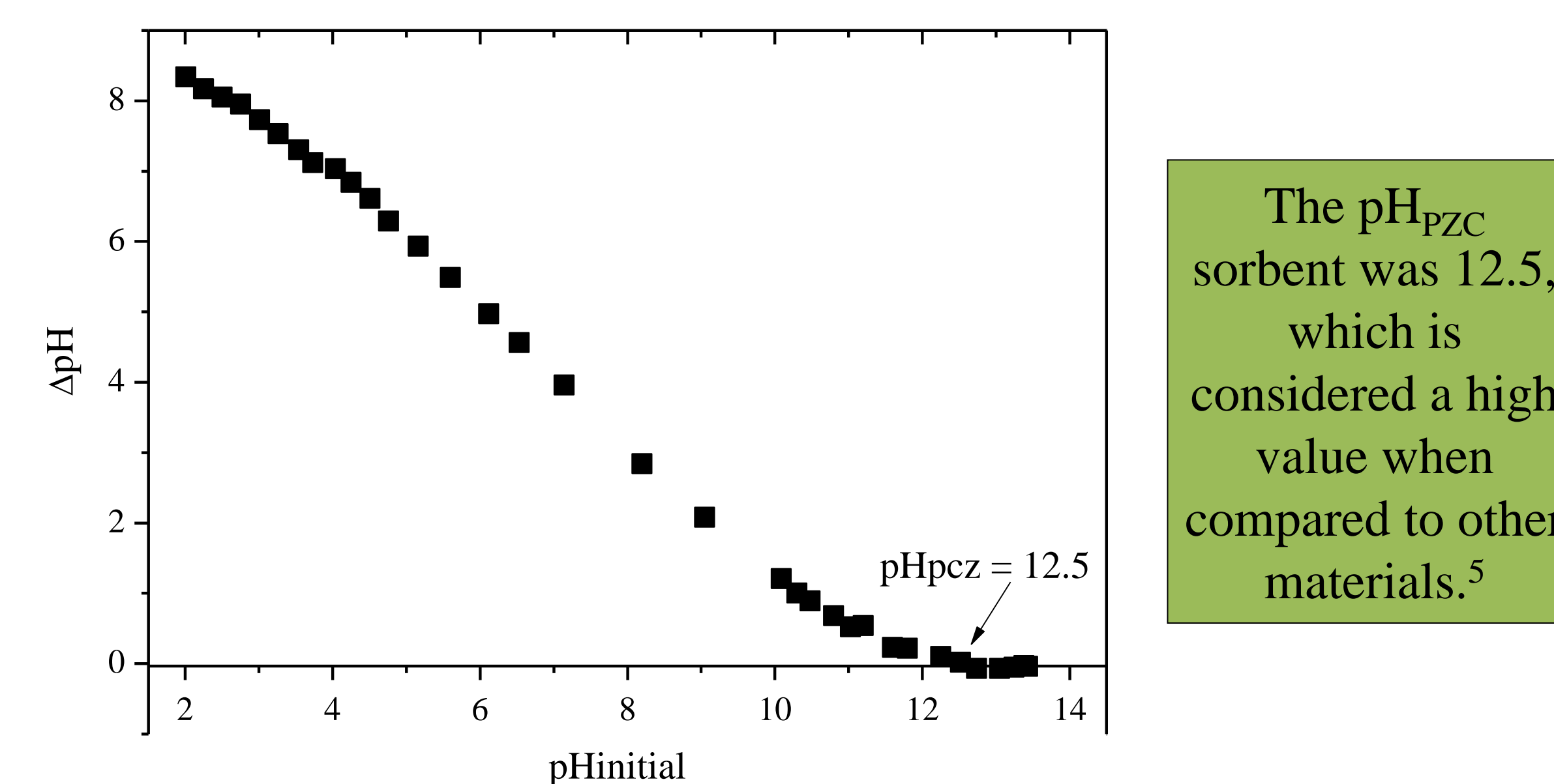


Figure 4: Point of zero charge (pH_{PZC}) of sorbent. Conditions: mass of sorbent 50.0 mg and temperature of 298K.

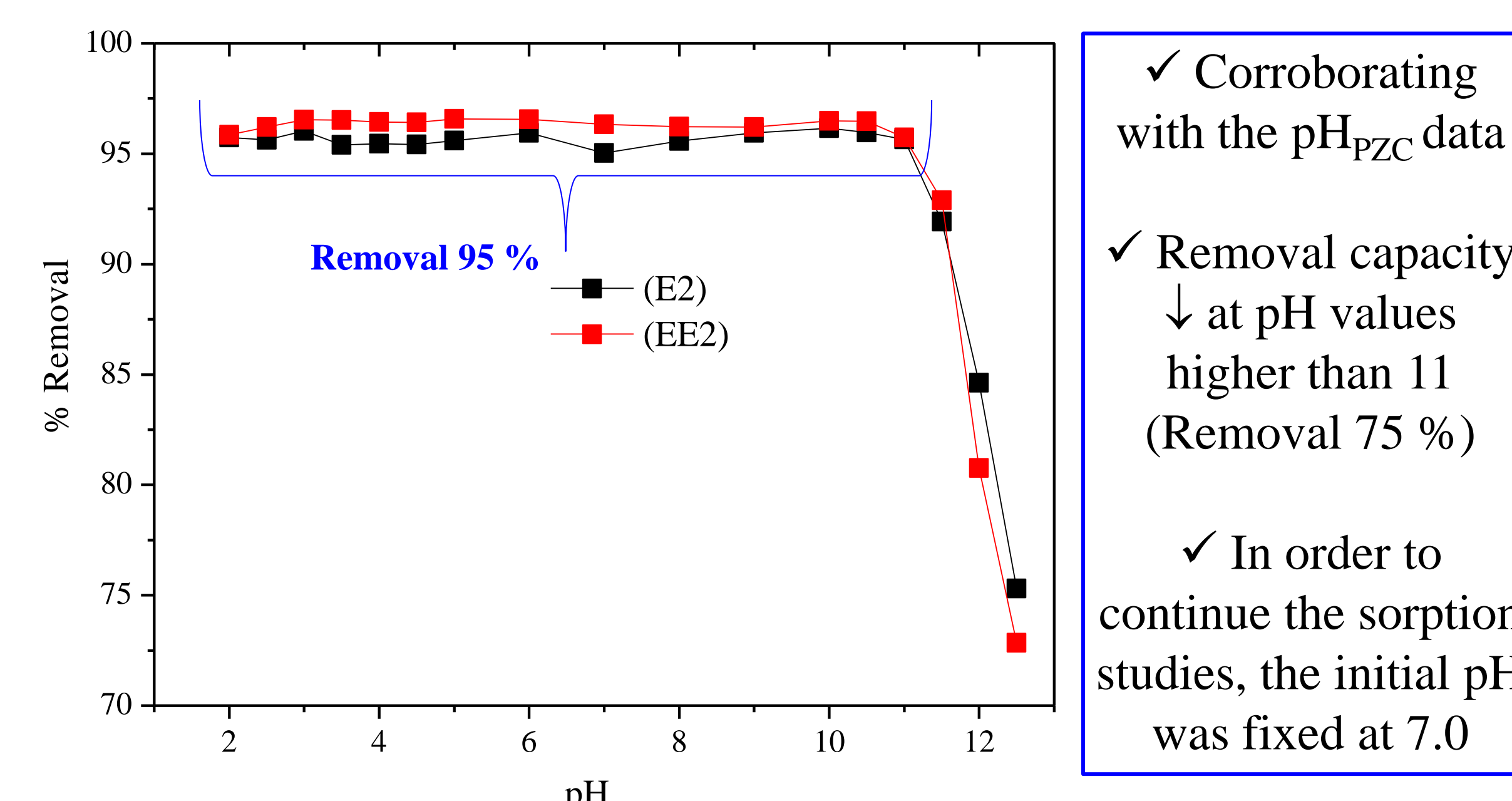


Figure 5: Effect of pH on the E2 and EE2 removal. Conditions: $\text{Co} = 2.00 \text{ mg L}^{-1}$ of E2 or EE2; temperature at 298K; mass of sorbent of 30.0 mg; time of contact 24 h.

Effect of Sorbent Dosage

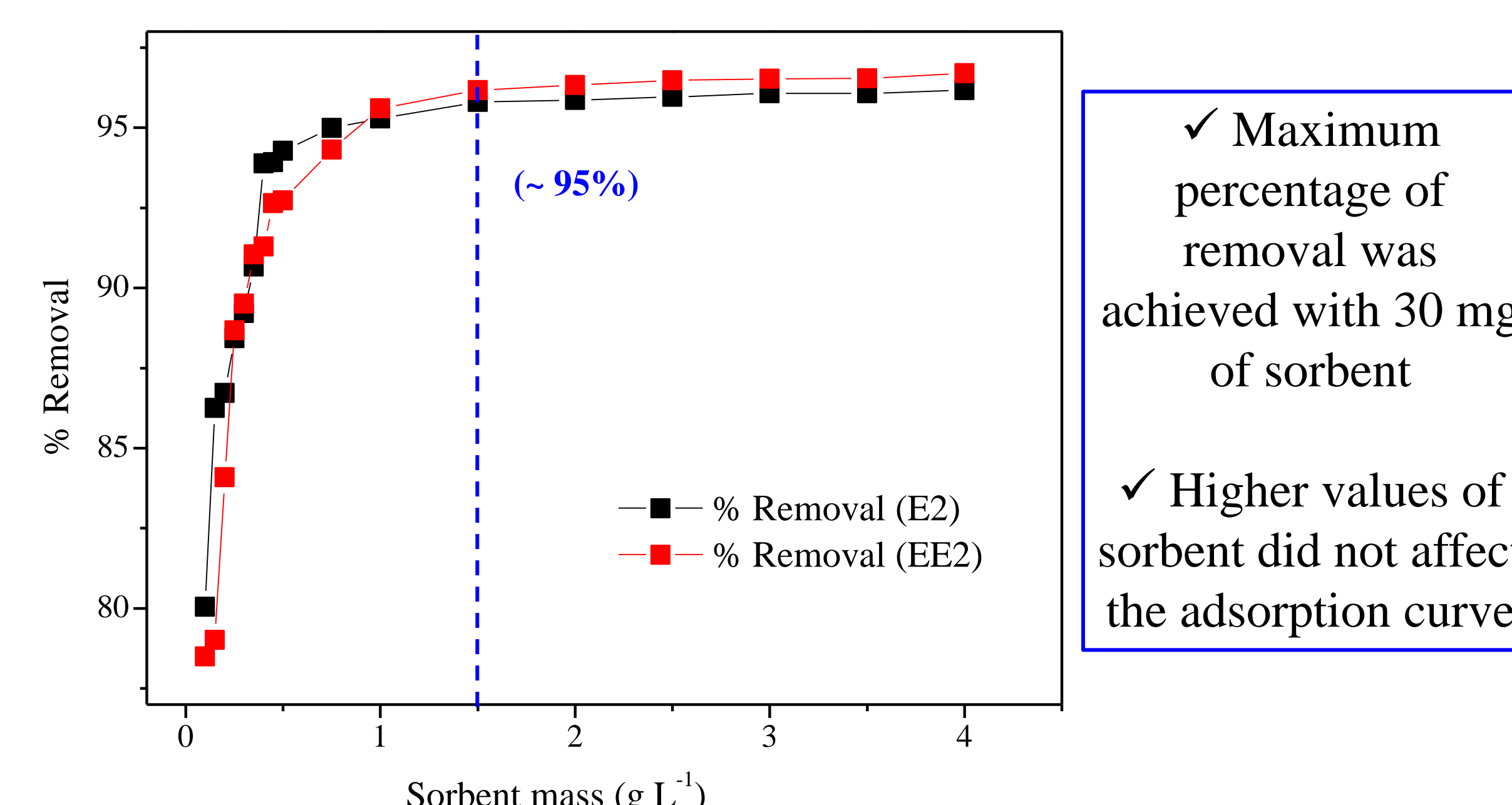


Figure 6: Effect of sorbent dosage on the E2 and EE2 removal. Conditions: $\text{Co} = 2.00 \text{ mg L}^{-1}$ of E2 or EE2; temperature at 298K; time of contact 24 h.

Effect of Time

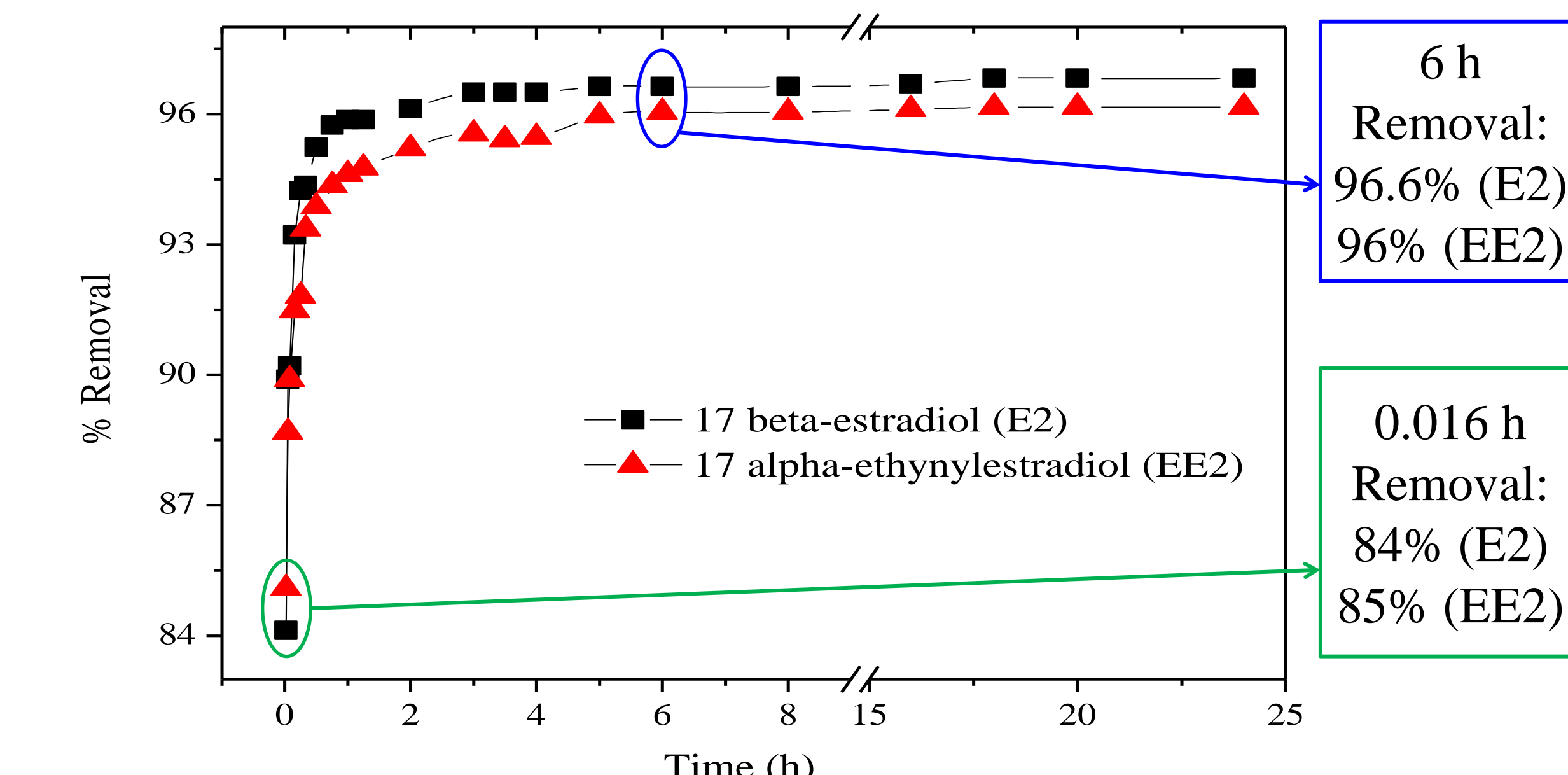


Figure 7: Effect of time on the E2 and EE2 removal. Conditions: $\text{Co} = 2.00 \text{ mg L}^{-1}$ of E2 or EE2; temperature at 298K; mass of sorbent of 30.0 mg; pH = 7.0.

Tabela 1: Kinetic parameters for EE2 and E2 removal using activated carbon adsorbent. Conditions: temperature was fixed at 298 K; pH 7.0, mass of adsorbent 30.0 mg, $\text{Co} = 2.00 \text{ mg L}^{-1}$.

Kinetic Parameters	(EE2)	(E2)
Pseudo-first-order		
$q_e (\text{mg g}^{-1})$	1.260	1.269
$k (\text{g mg}^{-1} \text{ h}^{-1})$	149.16	132.14
R^2	0.98795	0.98968
Pseudo-second-order		
$q_e (\text{mg g}^{-1})$	1.269	1.278
$k (\text{g mg}^{-1} \text{ h}^{-1})$	371.55	296.25
R^2	0.99388	0.99659
General order		
$q_e (\text{mg g}^{-1})$	1.319	1.297
$k (\text{g mg}^{-1} \text{ h}^{-1})$	15036	11090
n	4.911	3.125
R^2	0.99893	0.99895

CONCLUSION

➤ All experiments showed the potential of the agroindustrial sorbent as a new material for adsorption (EDC).

➤ The reuse of the agroindustrial waste for the adsorption of E2 and EE2 has some advantages over the commercial activated carbon as negligible commercial value, due to the fact that it is a waste of production processes.

ACKNOWLEDGEMENT

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